

Copper for artificial photosynthesis

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ETHYLENE

47.2 MJ/kg; 0.055 MJ/L

 $Ethylene \rightarrow Polyethylene$

(polyvinyl chloride, polystyrene)

Ethylene: 200 millions tons in 2018 (the largest of any organic chemical)

Currently

Steam cracking of naphta or saturated hydrocarbons (750-950°C)

Enormous energy inputs
 (8% de the total primary energy consumption in chemical industry)

> Production of 2 tons CO_2 / ton ethylene)

Artificial photosynthesis: two scenarios



- Technology still immature
- Solar-To-Fuels efficiency <1%</p>
- Low current densities (< 50 mA.cm⁻²)
- Integration > low tunability
- Light-degradation of catalysts
- Electrolyte-degradation of photoabsorber
- Integration > limited cost
 - Mobility (free of electricity source)



- Mature technologies
 - Closest to commercialization
 - > PV-electricity price: 0.03/kWh (\checkmark)
 - (the electricity cost is the largest expense)
 - Solar-To-Fuels yields 5-10 % (CO)
 - System separation: tunable
 (Independent optimization PV vs EC)
- PV to EC matching > cost

Artificial photosynthesis scenario : photovoltaics + electrolysis



- CATALYSIS

Homogeneous/molecular catalysts ? (which ligands? Which metal ions ?)

Heterogeneous/solid catalysts ?

Efficiency: Highest current density: > 0.2 A.cm⁻²

Lowest overpotential (cathode: 0.4-1 V vs anode 0.2-0.3 V at 10-50 mA.cm⁻²)

Stability (corrosion/deactivation)

Use the same catalyst at both electrodes Earth-abundant materials pH

Cost (the electricity costs are the largest contribution)



Heterogeneization of molecular complexes



Nanostructuration of surfaces Tailoring the morphology

- SOLVENT

Water (but low solubility of CO₂-30 mM) Mass transport limitations



Liquid phase electrolyzer

Continuous flow electrochemical cell Gas diffusion electrodes



Gas phase electrolyzer (Gas diffusion electrode)



Optimization with ≠ cations/anions Ionic liquids ?



Alkaline electrolysis ? Neutral electrolysis ?

Electrolyte

- SELECTIVITY

How to avoid/control H₂?

How to direct the reaction towards the desired product ? (product purification)



Control by the

- Catalyst (metal/morphology/ligand)
- Electrolyte
- Conductive support



- PRODUCTS

Liquid ? (ethanol, formic acid)

Gas ? (CO, CH₄,..)

2 e⁻ (CO,..) or ne⁻ (CH₄, C₂H₄..) products?



Fischer-Tropsch

CO (\$3B)

Economically unviable (high CAPEX)+ CO₂ emissions



New markets ?

HCO₂H (\$0.6B)



Fuel

CH₃OH Rarely observed in CO2RR



Hydrocarbons

CH₄ too cheap
Ethylene interesting (\$220B)
but currently cheap (shale ethane cracking)
Propylene very interesting



Alcohols

Ethanol very interesting (\$75B) + propanol + ethylene glycol

CO₂ reduction catalysis: Why Copper ?

CO2 Electrocatalysts Group 1 Group 18 **METALS** H 1s co He 1s² 1.0079 4.0026 Group 2 13 14 15 17 H2 10 3 9 Pt, Fe, Co H_2 F HC в N 0 Li 2st Be Ne 6.941 9.012 10.81 14.0067 15.999 18.998 20.179 нсоон Ag, Au, Pd, Zn, Ni 11 12 16 17 18 CO AI Ρ CI Na Mg Grou S Ar 39.948 22,989 24.305 30.974 32.06 35.453 12 Pb, Sn, Sn 20 21 34 35 36 HCO₂H 19 31 32 33 K Ca Sc V Mn Fe Co Ga Br Kr Ge As Se 39.098 40.08 44.956 69.72 72.59 74.922 78.96 79.904 83.8 37 54 38 39 43 51 52 53 Cu **Hydrocarbons** Y Rb Sr Zr Mo Tc Ru Pd Sb Te 1 Xe Ag 85.468 87.62 88.906 98 07 868 131.29 121.75 127.6 126.905 55 56 86 57 83 84 85 76 **Alcohols** Po Cs Ba La Та W Re Os Pt Au Pb Bi At Rn 132.905 137.33 222 138.906 107 87 88 89 104 105 106 Fr Ung Uns Ra Ac Unp Unh 223 226 025 227.028 262 26 262 263





Porous dendritic Cu-based material

Nanostructuring surfaces Tailoring the morphology



✓ macro/micro-porous structure (efficient mass transfer)
 ✓ high (electrochemical) surface area

Angew. Chem. 2017, <u>56</u>, 4792

Porous dendritic Cu-based material

The same catalyst for the anode and the cathode



A stable and efficient CO₂ reduction catalyst : Selective for **ethylene** formation

Proc. Natl. Acad. Sci. 2019, <u>116</u>, 9735

A stable and efficient O₂ evolution catalyst : 10 mA.cm⁻² at 280 mV overpotential (1M NaOH)

Angew. Chem. 2017, <u>56</u>, 4792

A flow electrochemical cell









From sun to hydrocarbons: photovoltaic + electrolyzer



PV coupled to Electrolyzer

perovskite solar cells

yield: 16.7% delivering 2.8 V



F. Bella

Ethylene C₂H₄ (35%) Ethane C₂H₆ (8%) H₂ 42%; HCOOH 6%; CO 5%

Current density 18 mA.cm⁻²

 $2 \operatorname{CO}_2 + 2 \operatorname{H}_2 \operatorname{O} \xrightarrow{} \mathbf{C}_2 \mathbf{H}_4 + 3 \operatorname{O}_2$

Solar-to-hydrocarbon efficiency : 2.3 %

Proc. Natl. Acad. Sci. 2019, 116, 9735-9740

From sun to hydrocarbons: photovoltaic + electrolyzer

photovoltaics	cathode	anode	electrolyte	product	solar to fuel efficiency (%)	partial current density (mA/cm ²) ^a
Si	Cu ₂ O- derived Cu	IrO _x	0.2 M KHCO ₃	C_2H_4	1.5	6.5
Si	In	IrO _x	1 М КНСО ₃	НСООН	1.4 - 1.8	N.R. ^b
Si + InGaN	In	Ni-O	3 М КНСО ₃	HCOOH	0.97	~ 0.4
SiGe	Ru-based polymer	IrO _x	0.1 M phosphate buffer (K ₂ HPO ₄ :KH ₂ PO ₄ = 1:1)	НСООН	4.6	~ 0.1
GaAs/InGaP	Pd/C	Ni	2.8 М КНСО ₃ /ВРМ/1.0 М КОН	HCOOH	10	~ 8
Si	Au	CoO_x	0.5 M KHCO3	CO	2.0	~ 1.5
$Cu(In_xGa_{1-x})(S_ySe_{1-y})_2$	Au	Co ₃ O ₄	0.5 M KHCO3	CO	4.23	N.R.
perovskite	Au	IrO ₂	0.5 M NaHCO ₃	CO	6.5	~ 1.4
Si	WSe ₂	Co-O/OH	50% EMIM-BF ₄ in water (cathode)/potassium phosphate buffer (anode)	СО	4.6	N.R.



Hydrophobicity and Nature

Nature has special mechanisms to keep gas trapped at a surface when submerged

Diving bell spider Plastron

Gas trapping is controlled by hydrophobic hairs called 'a plastron'

This allows the spider continue to breathe underwater

Can a similar effect be exploited for CO₂ reduction using hydrophobicity?



Controlled current electrolysis (30 mA.cm⁻²)

in 0.1 M CsHCO₃ with CO₂ at flow rate of 5 ml min⁻¹



Wettable dendrite requires –1.1 V vs. RHE *Hydrophobic* dendrite requires –1.5 V vs. RHE

Nature Materials 2019, <u>18</u>, 1222-1227

Flow of CO_2 on the hydrophobic dendrite













Angew. Chem. 2019, <u>58</u>, 15098-15103



Cu for conversion de CO₂ into Ethanol !!



Dilan Karapinar





Cu for conversion de CO₂ into Ethanol !!



Cu for conversion de CO₂ into Ethanol !!



> 55% FY ethanol from CO_2 electroreduction

Angew. Chem. 2019, <u>58</u>, 15098-15103

Operando in situ EXAFS





X-ray spectroelectrochemical setup used at the SAMBA beamline. RE, CE and WE stand for reference, counter and working electrode. SR stands for synchrotron radiation

Active sites: transient Cu nanoparticles ?



Operando XAS characterization of Cu-NC







Coupling CO*/CO*: formation of C-C bonds



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